$$f^* \propto = \frac{56A}{200 (K_{0W})^{0.84}} = \frac{35}{200 (8,128,305)^{0.84}} = \frac{3.75 \times 10^{-7}}{200 (8,128,305)^{0.84}}$$

$$f\alpha = 0.25\% = 0.0035$$

$$R = 1 + pd Kd = 1 + 1.55 g/cm^3 \times 345.1 mL/g$$
 n
 0.45

2) with advection dominant: plug flow, so full concentration
$$L = \frac{1.0 \pm 0.3}{1} = 1.3$$

$$V_S = \frac{1}{1} \times 10^{-9} \, \text{m/s} \times 1.3 = 2.89 \times 10^{-9} \, \text{m/s}$$

$$N_e = \frac{1 \times 10^{-9} \, \text{m/s}}{0.45} \times 1.3 = 2.89 \times 10^{-9} \, \text{m/s}$$

$$t = \frac{1.0 \text{ m}}{2.89 \times 10^{-9} \text{ m/s}} = 3.46 \times 10^8 \text{ s} = 11.0 \text{ years}$$

3) With dispusion dominant:

$$\frac{c}{c_0} = \operatorname{erfc}\left(\frac{x}{2\sqrt{D^*t}}\right) = 0.75 = \operatorname{erfc}\left(\beta\right)$$

$$\beta = 0.8$$
 gives eft $(\beta) = 0.758$ $0.258 - 0.229 = 0.029$ $\beta = 0.85$ gives eft $(\beta) = 0.729$ $0.008 \times 0.05 = 0.014$

$$0.25 = erfc(0.814)$$

$$0.814 = \frac{1 \text{ m}}{2 \int \frac{1.2 \times 10^{-10} \text{ m}^2/\text{s}}{1189.7} \times \text{t}}$$

$$D^* = 1.2 \times 10^{-10} \, \text{m}^2 \times 3600 \, \text{s} \times 24 \, \text{g} \times 365 \, \text{d} = 0.00378 \, \text{m}^2$$

$$0.814 = \frac{1 \text{ m}}{2 \int_{0.00378 \text{ m}^2/\text{yr}} \times t}$$

$$1189.7$$

$$t = 1 m = 1$$

$$4 \times 0.00378 \times 0.814 \times 0.814 = 0.00008421$$

$$1189.7 \times 0.814 \times 0.814 = 0.00008421$$

4) With advertion and dyfusion both important
$$C = 0.25 = \pm \begin{cases} ersk \left(\frac{Rx - \sqrt{st}}{2\sqrt{D^*R^*t}} + app \left(\frac{\sqrt{sx}}{2\sqrt{D^*R^*t}} \right) \\ \sqrt{sx} \\ D^* \end{cases}$$

$$\sqrt{sx}$$

$$V_{5} = 2.89 \times 10^{-9} \frac{m}{5} \times 3600 = \times 24 \frac{m}{2} \times 365 d = 0.0911 \frac{m}{4r}$$

$$V_{52} = 0.0911 \frac{m}{4r} \times 1 \frac{m}{2} = 24.1$$

$$D^{*} = 0.00378 \frac{m^{2}}{4r} = 24.1$$

$$exp(24.1) = 2.93 \times 10^{10}$$

$$R = 1189.7$$
 $D^{\dagger} = 0.06378$
 $V_S = 0.0911$

Consider efc $\frac{Rx + V_St}{2D^*RE}$
 $= efc(\beta)$

at t = 10 years
$$\beta = \frac{1189.7 \times 10 + 0.0911 \times 10}{2 \sqrt{0.00378 \times 1189.7 \times 10}}$$

= $\frac{11,897 + 0.911}{13.4} = 887.$

B is too large and will always be too large so the second term will always be qual to zero, so typnore the second term.

$$0.5 = efc(\beta)$$
; β between 0.45 and 0.5

4) contid.
$$\beta = 0.45$$
 exc $(\beta) = 0.524$ 0.524-0.480=0.044 $\beta = 0.480$ exc $(\beta) = 0.480$ 0.24 x 0.55 = 0.087 0.44 $\beta = 0.497$ exc $(\beta) = 0.50$

$$\frac{Rx - Vst}{2 \int D^*Rt} = \frac{1189.7 \times 1 - 0.0911 t}{2 \int 0.00378 \times 1189.7 \times t} = 0.477$$

for a day soil the grain eight may be from 0.001 to 6.005 mm according to ADTM D 4127 "Governironmental Engineering", Sharma and Raddy, 2004, p. 46.

 $V_{S} = 2.89 \times 10^{-9} \text{ m/s}$

 $D_0 = \frac{D^+}{C}$ where C ranges from 0.01 to 8.5 let C = 0.2

Do = 1.2 415-10 m2/5 = 6 410-10 m2/5

 $V_{Sd} = 2.89 \times 10^{-9} \text{ m/s} \times 2.5 \times 10^{-6} \text{ m} = 1.20 \times 10^{-5}$ $V_{Sd} = 2.89 \times 10^{-9} \text{ m/s} \times 2.5 \times 10^{-6} \text{ m} = 1.20 \times 10^{-5}$ $V_{Sd} = 2.89 \times 10^{-9} \text{ m/s} \times 2.5 \times 10^{-6} \text{ m} = 1.20 \times 10^{-5}$ $V_{Sd} = 2.89 \times 10^{-9} \text{ m/s} \times 2.5 \times 10^{-6} \text{ m} = 1.20 \times 10^{-5}$ So diffusion domination

6) Waste is represented by C68 HIII OSO N C68 HIII O50 N + (4x68 - 111 - 2x50 + 3x1) H20 > (4x68 + 111 - 2x50 - 3x1) CH4 + (4x68-111+2x50+3x1) (02 + NH3 C68 H111 OSON + 16 H20 > 35 CH2 + 33 CO2 + NH2 (68×12 816 16×(2+16) 35(12+4) 33(12+32) 14+3 50 × 16 800 1 × 14 14 560 1,452 1741 288 17 0,7177 Kg m3. 1000 kg $\frac{1000 \text{ kg}}{1741} = \frac{20 \text{ kg}}{560}$ 321.65 kg = 448 m3 0.7177 Kg m3 = 448,000 L CH3 = 321.65 kg. CH4



